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1	Behavior of a hemp-based concrete wall under dynamic thermal and hygric solicitations
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6	

7 Abstract

8 Here we document the behavior at wall scale of a hemp-based hygroscopic material under 9 various temperature and moisture dynamic conditions. The wall was made of precast hemp 10 concrete (HC) blocks with air cavities. It was tested within a bi-climatic chamber and monitored 11 thanks to hygrothermal sensors in the wall and in the chambers. The results from an in-house heat 12 and moisture transfer model were compared to the experimental data, using the actual thermal 13 and hygric characteristics of the hemp-based material determined in a previous study. The 14 experiments allowed to demonstrate how the heat and moisture transport phenomena within the 15 wall are coupled, particularly how a temperature difference can be a sufficient driving force for 16 the release of moisture. The work points out the impact of moisture adsorption on heat release 17 and on the temperature changes within the wall. Finally the numerical model served also to the 18 modelling of an equivalent wall made of concrete to help highlighting the moisture dumping 19 capability of the bio-based material, together with its thermal insulation capacity.

20 Keywords: heat and moisture transfer, bi-climatic chamber, wall scale, Hemp Concrete, bio-21 based materials.

22 Nomenclature

23 Latin symbols

24	Α	Aspect ratio	(-)
25	A_w	Soprtion coefficient	$(kg.m^{-2}.s^{-1/2})$
26	c_p	specific heat capacity	(J.kg ⁻¹ .K ⁻¹)
27	d	air layer thickness	(m)
28	g	gravitational force	(m.s ⁻²)
29	g_m	mass flux	$(kg.m^{-2}.s^{-1})$
30	h_c	surface heat transfer	(W.m ⁻² .K ⁻¹)
31	h_m	surface mass transfer	(kg.m ⁻² .s ⁻¹ .Pa ⁻¹)
32	Н	height	(m)
33	k	thermal conductivity	(W.m ⁻¹ .K ⁻¹)
34	L	length	(m)
35	L_{v}	latent heat	(J.kg ⁻¹)
36	Nu	Nusselt number	
37	p_c	capillary pressure	(Pa)
38	p_{v}	vapor pressure	(Pa)
39	$p_{v,sat}$	saturated vapor pressure	(Pa)
40	q_c	heat flux	(W.m ⁻²)
41	Ra	Rayleigh number	
42	RH	relative humidity	(-)
43	S_l	moisture source term	(kg.m ⁻³ .s ⁻¹)

44	Т	temperature	(°C or K)
45	t	time	(s)
46	V	velocity	(m.s ⁻¹)
47	W	total mass water content	(kg.m ⁻³)
48	W	width	(m)
49			
50	Greek s	symbols	
51	α	thermal diffusivity	$(m^2.s^{-1})$
52	β	thermal expansion coefficient	(K ⁻¹)
53	δ	permeability	(kg.m ⁻¹ .s ⁻¹ .Pa ⁻¹ or s)
54	ν	kinematic viscosity	$(m^2.s^{-1})$
55	ρ	density	(kg.m ⁻³)
56			
57	Subscripts		
58	f	free saturation	
59	НС	Hemp Concrete	
60	i	liquid or vapor	
61	l	liquid	
62	S	solid	
63	surf	surface	
64	v	vapor	
65			

66 **1** Introduction

Hemp Concrete (HC) belongs to the class of bio-based construction materials. It is made of the combination of hemp shiv particles with a binder, generally based on lime in order to maintain the hygroscopic properties of the resulting material. Hemp shiv is the woody core of the hemp stalk obtained through defibration by a mechanical breaking process. The terminology HC is typically used as an analogy to the usual concrete blocks used in construction. Nevertheless, one has to keep in mind that the basic component of concrete, cement, is not present within the HC composition.

74 Thanks to photosynthesis, bio-based materials can be called CO₂ storage materials. This 75 characteristics, together with the hemp hygrothermal properties developed thanks to the hemp 76 pore structure, make the HC an excellent candidate for meeting sustainable construction 77 objectives. Such materials are perceived as potential solution for energy efficient buildings with a 78 reduced carbon footprint. Controlling heat and moisture transfer through the buildings envelope 79 by using hygroscopic materials may bring a contribution not only on an energy point of view 80 (Osanyintola and Simonson, 2006, Woloszyn et al., 2009) but also on a health standpoint. The 81 increase in moisture content comes indeed with a rise in microorganism concentration 82 (Baughman and Arens, 1996), and the control of mold is directly related to the humidity level in 83 the buildings envelope.

The research field on bio-based construction materials is very active, both on the experimental side and on the modelling one. As far as the latter is concerned, heat and moisture numerical models rely on different driving potentials to describe the moisture exchanges: it can be either the moisture content or the capillary pressure or the vapor pressure. Therefore the final set of equations varies from one author to another one. Examples of models can be found in the works
Hagentoft et al. (2004), Li et al. (2009), Tariku et al. (2010), Steeman et al. (2010), Delgado et al.
(2013), or Van Belleghem et al. (2014). The main modelling challenge lies in the fluid flow
through the porous structure combined to phase change, making the set of equations to solve
highly non-linear. The issue is highlighted in Souza et al. (2008), Mahabaleshwar et al. (2017),
Salimpour et al. (2017), Husman et al. (2016), Pepe et al. (2017).

94 The experimental investigations rang from the sample scale to the building scale in real climatic 95 conditions. For example, detailed measurements were presented in Lelievre et al. (2014) on a 96 hemp-based element showing the thermo-hygric response to a change of relative humidity of the 97 environment. Wall scale laboratory experiments were performed by Aït Oumeziane et al. (2016) 98 in almost isothermal conditions. In 2018, Moujalled et al. published the results of an 99 experimental campaign of 4 years on a house which envelope was partially made of a sprayed 100 hemp and lime concrete, demonstrating the moisture buffering capacity of such material in real 101 life climatic conditions. This work came after the pioneering works of Shea et al. (2012) 102 performed on a rather smaller building based on different construction techniques.

103

The work presented in this paper is aimed at investigating the response of a wall made of a hempbased material to controlled dynamic solicitations in both temperature and humidity within a biclimatic chamber. The temperature and water vapor profiles obtained during the experimental campaign serve a three-fold purpose: one is to assess the moisture buffering capacity of such material, the other is to provide a set of HAM (Heat and Moisture) data necessary to the wallscale validation of a numerical model based on the finite elements method; the final one is to examine how the hemp-based wall behavior differentiates from a classical concrete wall in termsof thermo-hygric response.

112 **2** Experiments

113 **2.1** Hemp Concrete wall in the test chamber and metrology

114 Blocks of HC were assembled in order to constitute a wall of 2.3 m in height, 1.6 m in width and 115 20 cm in thickness. Each HC block had the following dimensions: length = 50.8 ± 1.04 cm, 116 thickness = 19.9 ± 0.09 cm, height = 20.3 ± 0.24 cm. The assembly was made thanks to thin 117 horizontal mortar layers (70% metakaolin and 30% hydrated lime, sand/binder = 5 and 118 water/binder = 0.6), while the vertical sides of the blocks were interlocked to each other (see Fig. 119 1 for the geometric features). The HC blocks contain air cavities (Fig. 1a). Due to the vibro-120 compaction fabrication process, the HC layers were slightly thicker at the bottom of the brick 121 (HC thickness = 2.55 ± 0.07 cm at the top of the brick against 2.72 ± 0.09 cm at the bottom) 122 while it was the opposite for the air layer (air thickness = 0.94 ± 0.07 cm at the top against $0.71 \pm$ 123 0.06 cm at the bottom). Mean values of HC layer thickness $(2.63 \pm 0.08 \text{ cm})$ and air layer 124 thickness $(0.82 \pm 0.07 \text{ cm})$ were considered in the numerical study.

The HC was initially characterized by measuring its physical, thermal and hygric properties: density, porosity, thermal conductivity, specific heat capacity, air and vapor permeability, sorption and desorption isotherms, capillary adsorption coefficient. The details of this work can be found in Seng et al. (2019a, 2019b) and were used here as input data in the numerical model. The relationship between the relative humidity and the moisture content is an important topic as in most cases hemp-based materials exhibit a strong hysteretic behavior between adsorption and desorption, while the temperature at which the sorption-desorption isotherm experiments are 132 conducted may also have impact (Aït Oumeziane et al., 2016). The results corresponding to the 133 HC tested in this study are provided in Fig. 2, showing that the sorption and desorption 134 measurements at 23°C and 45°C gather along one single curve, justifying the use of a unique 135 isotherm in the study.

- 136
- 137

Insert Figure 1

- 138
- 139

Insert Figure 2

140

141 The test environment was made of two climatic rooms; both were controlled in temperature and 142 relative humidity. Each room has a horizontal surface of L x W = 3.30 m x 1.60 m and a height of 143 H = 2.30 m. The HC wall was placed into a wooden frame in order to separate the two chambers. 144 Special attention was dedicated to avoid any humid air leakage through the frame or the wall-145 frame interface. Note that deflectors were installed so that the air blown into the chambers to 146 maintain the chosen boundary conditions was not directly oriented toward the wall.

147

The hygrothermal behavior of the HC wall was monitored with 10 hygrothermal sensors (Honeywell HIH-4602-C). Each hygrothermal sensor was equipped with a 2 wires integral precision RTD sensor for the temperature (precision: Class B, $\pm 0.3 + 0.005$ T °C), and a planar capacitor for the RH ($\pm 3.5\%$ RH).

152	The hygrothermal sensors were distributed along the thickness of the wall, at the wall mid-height,
153	in the air cavities inside the wall and against the wall (Fig. 3). One sensor was deported
154	horizontally (sensor 7) so that the one-dimensional aspect of the transfer could be checked. All
155	the sensors were connected to a data acquisition processor which returned the measurements to a
156	computer outside the bi-climatic chamber.

- 157
- 158

Insert Figure 3

159

160 **2.2** Tests summary

A first series of test consisted in measuring the hygrothermal response of the wall to a temperature step solicitation without any moisture exchange between the wall and its surrounding environment. To this sake, the 2 faces of the wall were coated with a vapor barrier. After an initial stabilization phase at 25°C in the 2 rooms, the temperature was steeply increased to 45°C on one side, and maintained to this value for about 4 days.

In a next series, one chamber represented outdoor conditions, while the opposite one (hot side) was meant to reproduce indoor conditions. The hot side was always maintained at a constant temperature. In one case, vapor was produced for 1 hour in order to model room occupancy; the cold side was kept at 6°C and RH = 80%. The test lasted about 4 days. In the other case, the cold chamber was submitted to a sinusoidal temperature signal with an average temperature of 14°C, a total temperature amplitude of 16°C and a period of 24 hours. The RH slightly fluctuated around 172 80%. The hot chamber RH was not controlled. The test lasted 6 days. Figure 4 summarizes the 3173 configurations.

174

Insert Figure 4

175 **3** Numerical study

176 **3.1** Heat and moisture transfer through the HC

The problem is described by the conservation laws written for the HC layers and for the air layers. Equations (1) to (3) present the moisture transfer, the energy transfer and the moisture phase change rate in time. A first version of the model considering only HC was published in Seng et al. (2017). In this paper the work was compared to experimental data obtained on a small sample of HC from Lelievre et al. (2014). Working with realistic boundary conditions at a much bigger scale with actual wall elements is the aim of the present study.

183 The set of equations was solved for three variables: the capillary pressure p_c , the temperature *T* 184 and the moisture source term S_l which corresponds to the amount of moisture stored or released 185 in time by the solid phase.

$$\frac{\partial w}{\partial p_c}\frac{\partial p_c}{\partial t} = -\nabla \left[\left(\delta_l + \delta_v \frac{\rho_v}{\rho_l} \right) \nabla p_c - \delta_v \left(\operatorname{RH} \frac{\partial p_{v,sat}}{\partial T} - p_v \frac{\ln \operatorname{RH}}{T} \right) \nabla T \right]$$
(1)

$$\left(\rho_{s}c_{p,s}+\sum_{i}w_{i}c_{p,i}\right)\frac{\partial T}{\partial t}=k_{HC}\nabla^{2}T-\left[\left(c_{p,l}-c_{p,\nu}\right)T-L_{\nu}\right]S_{l}-\sum_{i}w_{i}V_{i}c_{p,i}\nabla T$$
(2)

$$\left(\frac{1}{1 - \rho_{\nu}/\rho_{l}}\right)\frac{\partial w}{\partial t} = -\nabla(\delta_{l}\nabla p_{c}) + S_{l}$$
(3)

186 where *w* is the total moisture content, δ_l is the liquid permeability, δ_v is the vapor permeability, 187 ρ_v is the water vapor density, ρ_l is the liquid water density, p_v is the vapor pressure, p_{vsat} is the 188 saturated vapor pressure, ρ_s is the material apparent density, w_i (i = v for water vapor or i = l for 189 liquid water) is the moisture content, $c_{p,i}$ is the specific heat capacity of water vapor or liquid 190 water , k_{mat} is the material thermal conductivity, V_i is the velocity of water vapor or liquid water 191 and L_v is the latent heat of vaporisation.

192 The HC thermal and hygric properties were measured in Seng et al. (2019a) and Seng et al. 193 (2019b). The curved fitting parameters obtained by means of the GAB model (Anderson, 1946) 194 are provided in Table 1 together with a summary of the other material properties. Note that the 195 amount of transported water vapor or liquid water $w_i V_i$ can be defined by $w_v V_v = -\delta_v \nabla p_v$ and 196 $w_l V_l = \delta_l \nabla p_c$, and that the $\sum_i w_i c_{p,i} \approx w c_{p,l}$ due to the small value of w_v compared to w_l .

197

198 **3.2** Heat and moisture transfer through the air layers

199 The Rayleigh number of an air cavity is given by

$$Ra_d = \frac{g\beta\Delta Td^3}{\alpha\nu} \tag{4}$$

where g is the gravitational force, β is the thermal expansion coefficient written $\beta = 1/T$ as air was considered as an ideal gas, ΔT is the temperature difference between the two faces of the cavity, d is the air layer thickness, α is the air thermal diffusivity and ν is the air kinematic viscosity. It was assumed that the temperature difference ΔT within an air layer varies from 1°C to 5°C. The Rayleigh number based on d, Ra_d estimated with Eq. (4) was therefore lower than 300. With an air layer thickness d = 0.82 cm, the air cavity aspect ratio is A = H/d = 24.8, with H = 20.3 cm. As $Ra_d < 10^4$ and $5 \le A \le 80$, the Nusselt was evaluated with the expression provided by Zhao et al. (1997):

$$Nu = \left(1 - 0.00813277 \left(\frac{Ra_d}{A}\right) + 0.00723291 \left(\frac{Ra_d}{A}\right)^{1.08597}\right)^{0.279072}$$
(5)

Because $Nu \le 1$, only conductive transfer was considered through the air cavity. With no convective transfer effect and no liquid phase transfer in the air cavity, the resulting HAM equations are:

$$\frac{\partial w_{air}}{\partial p_c} \frac{\partial p_c}{\partial t} = -\nabla \left[\left(\delta_v \frac{\rho_v}{\rho_l} \right) \nabla p_c - \delta_v \left(\operatorname{RH} \frac{\partial p_{vsat}}{\partial T} - p_v \frac{\ln \operatorname{RH}}{T} \right) \nabla T \right]$$
(6)

$$\left(\rho_{air}c_{p,air} + w_{v}c_{p,v}\right)\frac{\partial T}{\partial t} = k_{air}\nabla^{2}T$$
(7)

$$S_l = 0 \tag{8}$$

212 where w_{air} is the water vapor content in air defined from the ideal gas law (Table 1).

213

214

Table 1 : HC and air properties used in the numerical study

Parameter	Hemp Concrete (from Seng et al., 2019a, Seng et al. 2019b)	Air

Density	$\rho_{HC} = 466.2 \text{ kg.m}^{-3}$	$\rho_{air} = 1.2 \text{ kg.m}^{-3}$
Thermal conductivity	$k_{HC} = 0.112 \text{ W.m}^{-1}.\text{K}^{-1}$	$k_{air} = 0.026 \text{ W.m}^{-1}.\text{K}^{-1}$
Specific heat capacity	$c_{p,HC} = 905 \text{ J.kg}^{-1}.\text{K}^{-1}$	$c_{p,air} = 1004 \text{ J.kg}^{-1}.\text{K}^{-1}$
	GAB model $W_{HC} = \frac{\rho_{HC} \cdot u_m \cdot C \cdot K \cdot RH}{(1 - K \cdot RH)(1 + K(C - 1)RH)}$	Water vapor considered as an ideal gas $w_{air} = \frac{RH \cdot p_{v,sat}(T)}{R_v T}$
Isotherm	$\begin{array}{ccc} u_m & 0.0182 \\ C & 18.048 \\ K & 0.8219 \end{array}$	where R_v is the water vapor specific gas constant ($R_v = R/M_v$)
	(NB: the curve-fitting parameters correspond to a temperature of 23°C in adsorption)	$R = 8.314 \text{ J.mol}^{-1}.\text{K}^{-1}$ $M_v = 18 \ 10^{-3} \text{ kg.mol}^{-1}$
Water vapor permeability	$\delta_{v,HC} = 9.67 \ 10^{-11} \ \text{kg.m}^{-1}.\text{s}^{-1}.\text{Pa}^{-1}$	$\delta_{v,air} = 1.95 \ 10^{-10} \ \text{kg.m}^{-1}.\text{s}^{-1}.\text{Pa}^{-1}$
Liquid permeability	$\delta_{l,HC} = D_w \frac{\partial w}{\partial RH} \frac{RH}{\rho_l R_v T}$ where $D_w = 3.8 \left(\frac{A_w}{w_f}\right)^2 1000^{\frac{w}{w_f} - 1}$ $A_w = 0.139 \text{ kg.m}^{-2}.\text{s}^{-1/2}$	$\delta_{l,air} = 0 \text{ kg.m}^{-1}.\text{s}^{-1}.\text{Pa}^{-1}$
	$w_f = 541 \text{ kg.m}^{-3}$	

215

216 **3.3 Boundary conditions**

The thermal boundary conditions between the wall and the air in the climatic chambers were described with a convective heat flux q_c (W.m⁻²) in which the chamber temperature, T_{air}, may vary in time.

$$q_c = h_c (\mathrm{T}_{\mathrm{surf}} - \mathrm{T}_{\mathrm{air}}) \tag{9}$$

220 where h_c is the convective heat transfer coefficient.

221 The hygric boundary conditions were given by a convective mass transfer flux g_m , in which h_m 222 is the convective mass transfer coefficient.

$$g_m = h_m (p_{v,surf} - p_{v,air}) \tag{10}$$

The convective heat transfer coefficient was determined based on the air velocity v_{air} (m.s⁻¹) using a correlation of NF EN 15026 (AFNOR, 2008). The convective mass transfer coefficient was established with the heat and mass transfer analogy used by the same reference.

The air velocity was measured in the bi-climatic chamber; the corresponding convective heat andmass transfer coefficients are given in Table 2.

228

Table 2: Convective heat and mass transfer coefficients

Cold chamber	Hot chamber
$v_{air} = 5.3 \text{ m.s}^{-1}$	$v_{air} = 5.1 \text{ m.s}^{-1}$
$h_c = 23.5 \text{ W.m}^{-2}.\text{K}^{-1}$	$h_c = 22.85 \text{ W.m}^{-2}.\text{K}^{-1}$
$h_m = 1.21 \ 10^{-7} (\text{kg.m}^{-2}.\text{s}^{-1}.\text{Pa}^{-1}).$	$h_m = 1.18 \ 10^{-7} (\text{kg.m}^{-2}.\text{s}^{-1}.\text{Pa}^{-1}).$

229

230 **3.4** Numerical procedure

The model based on Eqs. (1)-(3) and Eqs. (6)-(8) was implemented in a FEM software, using the Partial Differential Equations module (COMSOL, 2017). The boundary conditions were set according to Eqs. (9) and (10): the air temperature and vapor pressure came from the measurement in the middle of the chamber (sensor 1 and 10, see Fig.3). A mesh sensitivity was performed this way: the maximum element size was set initially to 4 mm (corresponding to 114 elements) and divided by two one run after the other. We observed the temperature and the capillary pressure in the positions corresponding to the sensors shown in Fig.3. The error from one mesh to the other one was lower than 2.5% when the maximum element size was 0.25 mm which corresponded to 808 elements. We selected the case with the next step mesh refinement, i.e. with elements of maximum 0.125 mm leading to a mesh of 1600 elements.

At the interface between HC and air cavity, we considered temperature and capillary pressure continuity (Eqs. (11) and (12)).

$$T_{air} = T_{HC} \tag{11}$$

$$p_{c,air} = p_{c,HC} \tag{12}$$

243

244 **4 Results and Discussions**

245 **4.1 Moisture exchange potential**

The experimental results obtained in the presence of the vapor barriers are presented in Fig. 5 together with the simulations results after 1, 12 hours and 90 hours. The temperature and vapor pressure measured at the start of the test were used as initial conditions in the numerical model. One hour after the right-hand side (hot) chamber temperature was increased to 45°C, a temperature profile typical to heat diffusion was measured within the wall. The conductive heat wave propagated towards the opposite side until a linear temperature profile was reached after about 90 hours. The temperature gradient occurring on the right hand side of the wall comes with a vapor pressure gradient of the same sign. Because the two vapor barriers ensure that no moisture uptake happens from the climatic chambers, the vapor pressure increase in the material was due only to a moisture release from the bio-based material. The desorption of water molecules happened from right to left, and stopped after 90 hours as depicted by the horizontal vapor pressure profile.

The release of vapor was activated by the temperature gradient. The temperature profile was almost linear after 12 hours, while it took about 90 hours for the moisture to be released and the water vapor pressure profile to become horizontal. Once the temperature change stopped, the moisture gradient was a strong enough driving force to generate an additional release of vapor by the solid phase towards the left-hand side of the wall.

The numerical results reproduce the thermo-hygric behavior with a good accuracy. It is worth pointing out that the numerical temperature profile is the result of heat transfer by conduction through the wall combined to the latent heat contribution that accompanies the release of water molecules by the hemp-based matrix (see Eq. (2)). The scale analysis of heat and moisture transfer conducted in Seng et al. (2017) demonstrated that, for the range of temperature and humidity tested here, the third term in the right-hand side of the energy conservation was negligible.

270

271

Insert Figure 5

4.2 Occupancy in winter conditions

This situation corresponds to the presence of an occupant within the right-hand side (hot) chamber for 1 hour leading to a peak in RH while the ambient temperature remained constant. The cold chamber was maintained at 6 °C. Figure 6 shows the temperature and moisture measurements in time on the wall surface (hot chamber side) and within the wall. The ambient conditions (hot chamber) are shown in Fig. 6a, while Fig. 6b and c show the response at respectively about 3 cm (sensor 8) and about 6.5 cm (sensor 6) from the hot surface.

The vapor production happened a little bit before the start of the 3rd day of test. Because the 280 281 ambient temperatures had been maintained constant on both sides of the wall, the latter was in 282 thermal equilibrium when vapor started to be produced. Yet, Fig. 6b exhibits a temperature bump 283 of about 1°C at 3 cm from the hot surface which cannot be attributed to the thermal conditions. 284 Indeed, the adsorption of molecules of water vapor onto a hydrophilic surface comes with a heat 285 released. The enthalpy of adsorption, which depends on the type of solid surface, generates a 286 temperature increase detected by the sensors. Figure 6 indicates that this exothermic property of 287 water molecules adsorption was well predicted by the numerical model. Moving deeper into the 288 wall, the vapor pressure peak continued to appear but with a time lag: the increase in vapor 289 pressure and temperature was detected by the sensor at 3cm in the wall as soon as vapor was 290 produced in the hot chamber. A few centimeters deeper into the wall (sensor 6) a bump in vapor 291 pressure and in temperature remains noticeable but more centered towards Day 3, while its 292 amplitude decreased as the bio-based material kept adsorbing moisture. Consequently, as less 293 vapor was adsorbed onto the surface of the hemp fibers, the resulting peak temperature also 294 decreased. The numerical model describes coherently the thermos-hygric behavior even though 295 the temperature evolution in time are 1 °C below the measured values.

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- 298

297

299 4.3 Sinusoidal solicitations

Sinusoidal temperature and moisture solicitations tests are yet another way to assess the dynamic behavior of the HC. The results presented in this section correspond to a moment when a steady periodic regime is established. As shown in Fig. 4c, the sinusoidal temperature in the left-hand side (cold) chamber had a period of 24 hours. The RH was set to slightly fluctuate around 80%. There was a small overall increase of RH along the 6 days of test, around 1% per cycle. The temperature in the hot chamber was maintained at 24°C, and maintained constant throughout the test which lasted one week. The RH was left free to vary in this chamber.

307 The measurements in the 2 chambers are plotted in Fig. 7 in terms of vapor pressure and 308 temperature. Note that in the cold chamber the temperature peaks correspond as expected to the 309 vapor pressure peaks (Fig. 7a). As shown in Fig. 7b, the vapor pressure change in the hot 310 chamber also followed a sine wave in time, but with a much smaller amplitude than the one of the 311 vapor pressure in the cold chamber. This amplitude remained unchanged over the course of the 312 test, the vapor pressure ranging between 1000 and 1445 Pa. The RH corresponding to that evolution was between 34% and 48%. The period was also 24 hours. Moisture was absorbed by 313 314 the wall, and its peak was detected in the opposite chamber about 4.3 hours after the moisture 315 peak solicitation.

Figure 8 provides the temperature and vapor pressure changes in time at 3 different locations within the wall: in the vicinity of the left-hand side (cold) chamber where the ambient was controlled, at mid-distance within the wall, and in the vicinity of the hot chamber. In this figure, all the plain lines correspond to experimental results, while the dotted lines are for the numerical results.

The 3 sensors measured a steady periodic response of the temperature within the wall. The amplitude of the sine wave is higher in the vicinity of the cold side, and almost linear next to the opposite side where the ambient temperature was maintained constant.

324 Figure 8 shows how the sinusoidal variation in vapor pressure is transmitted from the cold side to 325 the warm chamber. The vapor pressure flow goes from the cold side to the hot one, as a sine 326 wave which amplitude decreases while approaching the hot chamber, as indicated by the 327 experimental values. Because only the cold chamber was controlled in relative humidity, a wall 328 made of a material with less hygroscopic properties would let the relative humidity in the hot 329 chamber increase in time. In the case of a wall made of HC, part of the water vapor is trapped 330 within the material and this moisture damping property explains the lower vapor pressure 331 amplitude on the hot side.

Plotted in Fig. 8 are also the numerical results obtained for the simulation of the HC wall. Note the good agreement between the numerical results and the experimental ones. This final validation of the model allowed to consider with confidence the case of a classical wall made of a material with non-hygroscopic properties with the purpose of differentiating thermal and hygric behaviors.

337 To this sake, we chose to model a wall made of a classic plain concrete. Concrete has a thermal 338 conductivity more than 10 times higher than the HC one, with a similar specific heat capacity. In 339 addition to being more thermally conductive, a typical concrete is also much less hygroscopic. 340 The concrete properties are provided in the EN 15026 norm (AFNOR, 2008). The initial and 341 boundary conditions were identical to the ones used in the modelling of the experiment. The 342 results corresponding to the simulation of the concrete wall were added to Fig. 8. The vapor pressure wave decreases in amplitude when moving from the cold chamber to the hot one. Yet 343 344 the amplitude is larger than in the case of HC. The concrete wall clearly does not have the same 345 damping property as the hemp-based wall. Figure 8 also highlights the lower moisture buffering 346 capacity of concrete: its peak of vapor pressure is less delayed that for the HC, meaning that the 347 moisture wave travels faster than for the hemp-based wall. As expected, the same result is 348 obtained for heat transfer. Figure 8c shows that the thermal wave is still present in the case of the 349 plain concrete wall in the vicinity of the hot chamber. These results highlights the potential of 350 HC as a material suitable for thermal comfort: relatively to a classical concrete-based wall, the 351 hemp-based wall is able to dampen moisture changes while demonstrating a good thermal 352 insulation.

353 **5** Concluding remarks

In this paper, the hygrothermal behavior of a wall made of precast HC blocks in a bi-climatic chamber was measured in different boundary conditions corresponding to realistic situations. The experimental data were compared to the numerical results obtained from a model based on FEM. The hygrothermal properties of the HC came from the works of Seng et al. (2019a, 2019b). The numerical model, once validated, was used as a comparison tool with a typical wall made of plain

360	the wall. The	study highlighted:	
361	- The p	potential for the hemp-based wall to release moisture under an applied temperature	
362	differ	rence while water exchange with the ambient is prevented.	
363	- The a	bility to adsorb a sudden peak of humidity from the ambient environment within a	
364	few h	iours,	
365	- The c	capacity, unlike a concrete-based wall, to dampen a thermal and hygric sinusoidal	
366	solici	tation, decreasing the moisture wave amplitude from one chamber to the other one,	
367	while	e delaying its travel through the wall.	
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369			
370	Acknowledg	gements:	
371	Billy Seng's	PhD thesis was funded by the NeOCampus research project.	
372			
373	Figures caption		
374	Figure 1	(a) HC block, (b) HC wall (built by Vu et al., 2015), and (c) wall instrumented	
375		with hygrothermal sensors.	
376	Figure 2	Sorption and desorption isotherm of the HC at 23°C and 45°C, adapted from Seng	
377		et al. (2019b).	
378	Figure 3	Hygrothermal sensors in the bi-climatic chamber: (a) side view of the bi-climatic	
379		chamber, (b) top view of the sensors installation.	

concrete, in the case of a dynamic solicitation in temperature and vapor pressure on one side of

Figure 4 The different experimental configurations: (a) the wall is coated with a vapor barrier on each side and submitted to a temperature difference between the 2 ambiences, (b) 1 hour of vapor production in one chamber simulates the presence of an occupant indoor, the outside is meant to represent winter conditions, and (c) a sinusoidal temperature solicitation with constant RH in the cold chamber while the other chamber is maintained at constant temperature.

- Figure 5 Temperature and vapor pressure distribution within the wall when the wall is
 coated by a vapor barrier on its both sides. (a) initial conditions, after (a) 1 hour,
 (b) 12h (b) and (c) 90 hours.
- Figure 6 Temperature and vapor pressure evolution in time (a) in the hot chamber, (b) at 3 cm and (c) at 6.5 cm from the hot side. The solicitation is meant to resemble the moisture production that an individual would produce during 1 hour of room occupancy. The plain lines are for the experimental results, while the dotted lines correspond to the experimental ones.
- Figure 7 Temperature and vapor pressure changes in time in (a) the hot chamber and (b) the cold chamber when the cold side is submitted to sinusoidal temperature with ~ constant RH and the hot side is simply maintained at constant temperature. The plain lines are for the experimental results, while the dotted lines correspond to the experimental ones.
- Figure 8 Temperature and vapor pressure changes in time within the material at (a) 3 cm
 from the cold side, (b) mid wall thickness and (c) 6.5 cm from the hot side, when
 the boundary conditions are those of Fig. 7. The experimental curves are

- 402 completed by the numerical ones in the case of the HC wall and for a similar wall
- 403 made of concrete. The plain lines are for the experimental results, while the dotted
- 404 lines correspond to the experimental ones.
- 405
- 406

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Figure 1



Figure 2



Block 2

Cold chamber

Hygrothermal sensor •

Figure 3









Figure 4



Figure 5



Figure 6



Figure 7



Figure 8